

Some Relationships for Gases

define some units

these are extracted from Van Wylen & Sonntag, Fundamentals of Classical Thermodynamics, Third Edition to which page numbers and equation numbers apply 2006: included reference to text: Woud section 2.23 in [W n.nn]

$$\text{kJ} := 10^3 \cdot \text{J}$$

$$\text{kmol} := 10^3 \text{ mole}$$

section 3.4 Equations of state for the vapor phase of a simple compressible substance - page 41 (Woud page 20)

gas at low density (experiment) $p \cdot \bar{v} = \bar{R} \cdot T$ $\bar{R} = \text{universal_gas_constant}$ (3.1)

$$\bar{R}_{\text{bar}} := 8.3144 \frac{\text{kJ}}{\text{kmol} \cdot \text{K}}$$

units sometimes ... $\frac{\text{kJ}}{\text{kg} \cdot \text{mol} \cdot \text{K}}$

$$R = \frac{\bar{R}}{\text{mw}}$$

mw = molecular_weight

for \bar{R}_{bar} above

$$\text{mw} = \frac{\text{kg}}{\text{kmol}}$$

$$p \cdot V = m \cdot R \cdot T$$

or ...

$$p \cdot v = R \cdot T \quad (3.2)$$

$$\frac{p_1 \cdot v_1}{T_1} = \frac{p_2 \cdot v_2}{T_2} \quad (3.5)$$

[W 2.32, 2.33]

section 4.3 Work done at moveable boundary of simple compressible system - page 63

if ... $p \cdot V^n = \text{constant}$ $n = 1$ $W_{1-2} = \int_{V_1}^{V_2} p \, dV = p_1 \cdot V_1 \cdot \int_{V_1}^{V_2} \frac{1}{V} \, dV = p_1 \cdot V_1 \cdot \ln\left(\frac{V_2}{V_1}\right)$ (4.5)

section 5.6 The Constant-Volume and Constant-Pressure Specific Heats - page 98

specific heat = increment of heat Q to change T by 1 deg

$$c = \frac{1}{m} \cdot \frac{\delta Q}{\delta T} \quad \frac{1}{m} = \text{specific}$$

two cases: 1) constant volume

$$c_v = \frac{1}{m} \cdot \frac{\delta Q}{\delta T} \quad \text{constant volume}$$

1st law ... $\delta Q = dE + \delta W = dU + dKE + dPE + \delta W$ (5.4)

$$\delta Q = dU + p \cdot \delta V \quad dKE = dPE = 0 \quad \delta W = p \cdot \delta V = 0$$

$$c_v = \frac{1}{m} \cdot \frac{\delta Q}{\delta T} = \frac{1}{m} \cdot \frac{\delta U}{\delta T} = \frac{\delta u}{\delta T} \quad c_v = \frac{\delta u}{\delta T} \quad \text{constant volume} \quad (5.14) \quad [\text{W 2.36}]$$

2) constant pressure

$$\delta Q = dU + p \cdot \delta V = \delta H \quad \text{as } \dots \quad dH = d(U + p \cdot V) = dU + p \cdot dV + V \cdot dp \quad dp = 0$$

$$c_p = \frac{1}{m} \cdot \frac{\delta Q}{\delta T} = \frac{1}{m} \cdot \frac{\delta H}{\delta T} = \frac{\delta h}{\delta T} \quad c_p = \frac{\delta h}{\delta T} \quad \text{constant pressure} \quad (5.15) \quad [\text{W 2.37}]$$

section 5.7 The Internal Energy, Enthalpy and Specific Heats of Ideal Gases - page 100

ideal gas $p \cdot v = R \cdot T$ $u = f(T)$ experiment (Joule)

$c_v = \frac{\delta u}{\delta T}$ u not a function of $v \Rightarrow$ $du = c_{vo} \cdot dT$ $v_o \Rightarrow$ constant volume ideal gas (5.20)

also ... $h = u + p \cdot v = u(T) + R \cdot T = h(T)$ i.e. $h = F(T)$ only

$c_p = \frac{\delta h}{\delta T} \Rightarrow dh = c_{po} \cdot dT$ $p_o \Rightarrow$ constant pressure ideal gas (5.24)

relation between c_{vo} and c_{po} ... $h = u + pv = u + R \cdot T$ $\frac{dh}{dT} = \frac{du}{dT} + R$ differentiate w.r.t T

$c_{po} = c_{vo} + R$ or ... $c_{po} - c_{vo} = R$ (5.27)

with constant c $h_2 - h_1 = c_{po} \cdot (T_2 - T_1)$ otherwise integrate if $c(T)$ known or tables (5.29) [W 2.38]

section 7.10 Entropy Change of an Ideal Gas - page 206

$T \cdot ds = du + p \cdot dv$ (7.7) [W 2.18]

$du = c_{vo} \cdot dT$ and ... $p \cdot v = R \cdot T \Rightarrow p = R \cdot \frac{T}{v} \Rightarrow T \cdot ds = c_{vo} \cdot dT + R \cdot \frac{T}{v} \cdot dv$

$ds = c_{vo} \cdot \frac{dT}{T} + R \cdot \frac{dv}{v}$ (7.19) $s_2 - s_1 = c_{vo} \cdot \ln\left(\frac{T_2}{T_1}\right) + R \cdot \ln\left(\frac{v_2}{v_1}\right)$ (7.24) $c_{vo} =$ constant otherwise integrate or use tables

$T \cdot ds = dh - v \cdot dp$ (7.7) [W 2.21]

$dh = c_{po} \cdot dT$ and ... $p \cdot v = R \cdot T \Rightarrow v = R \cdot \frac{T}{p} \Rightarrow T \cdot ds = c_{po} \cdot dT - R \cdot \frac{T}{p} \cdot dp$

$ds = c_{po} \cdot \frac{dT}{T} - R \cdot \frac{dp}{p}$ (7.21) $\Rightarrow s_2 - s_1 = c_{po} \cdot \ln\left(\frac{T_2}{T_1}\right) - R \cdot \ln\left(\frac{p_2}{p_1}\right)$ (7.23) $c_{po} =$ constant otherwise integrate or use tables

page 211 introduce specific heat ratio γ

$$\gamma = \frac{c_{po}}{c_{vo}} \quad (7.30) \quad [W 2.44] \quad \gamma = \gamma(T) \quad \text{as ...} \quad c = c(T)$$

from above $c_{po} - c_{vo} = R$ $c_{vo} = c_{po} - R = \gamma \cdot c_{vo} - R \Rightarrow c_{vo} \cdot (1 - \gamma) = -R$

changing signs ...

$$c_{vo} = \frac{R}{\gamma - 1} \quad (7.31)$$

similarly ...

$$c_{po} - c_{vo} = R \quad c_{po} = R + c_{vo} = R + \frac{c_{po}}{\gamma} \Rightarrow c_{po} \cdot \left(1 - \frac{1}{\gamma}\right) = R = c_{po} \cdot \frac{\gamma - 1}{\gamma}$$

$$c_{po} = R \cdot \frac{\gamma}{\gamma - 1} \quad (7.31)$$

for **constant** specific heat = perfect gas

reversible, adiabatic process ... $T \cdot ds = du + p \cdot dv = 0$ reversible, adiabatic ...

$$du + p \cdot dv = c_{vo} \cdot dT + p \cdot dv \quad p \cdot v = R \cdot T \Rightarrow dT = \frac{1}{R} \cdot (p \cdot dv + v \cdot dp)$$

$$0 = c_{vo} \cdot dT + p \cdot dv = \frac{c_{vo}}{R} \cdot (p \cdot dv + v \cdot dp) + p \cdot dv = \frac{c_{vo}}{R} \cdot (p \cdot dv + v \cdot dp) + p \cdot dv = \frac{R}{\gamma - 1} \cdot \frac{1}{R} \cdot (p \cdot dv + v \cdot dp) + p \cdot dv$$

$$\Rightarrow (p \cdot dv + v \cdot dp) + p \cdot dv(\gamma - 1) = v \cdot dp + \gamma \cdot p \cdot dv = 0 \Rightarrow \frac{dp}{p} + \gamma \cdot \frac{dv}{v} = 0 \quad \text{dividing by } pv$$

integrating ... $\ln(p) + \gamma \cdot \ln(v) = \text{constant}$ or ... $p \cdot v^\gamma = \text{constant}$ (7.32) [W 2.49]

rearranging ... $\frac{p_2}{p_1} = \left(\frac{v_1}{v_2}\right)^\gamma$

for ideal gas $\frac{p_1 \cdot v_1}{T_1} = \frac{p_2 \cdot v_2}{T_2} \Rightarrow \frac{v_1}{v_2} = \frac{p_2 \cdot T_1}{T_2 \cdot p_1} = \frac{T_1 \cdot p_2}{T_2 \cdot p_1} \Rightarrow$

$$\frac{p_2}{p_1} = \left(\frac{v_1}{v_2}\right)^\gamma = \left(\frac{T_1 \cdot p_2}{T_2 \cdot p_1}\right)^\gamma = \left(\frac{T_1}{T_2}\right)^\gamma \cdot \left(\frac{p_2}{p_1}\right)^\gamma \Rightarrow \left(\frac{p_2}{p_1}\right)^{1-\gamma} = \left(\frac{T_1}{T_2}\right)^\gamma \quad \frac{p_2}{p_1} = \left(\frac{T_1}{T_2}\right)^{\frac{\gamma}{1-\gamma}} = \left(\frac{T_2}{T_1}\right)^{\frac{\gamma}{\gamma-1}}$$

and ... for reversible adiabatic process constant specific heat (ideal gas)

$$\frac{T_2}{T_1} = \left(\frac{p_2}{p_1}\right)^{\frac{\gamma-1}{\gamma}} = \left(\frac{v_1}{v_2}\right)^{\gamma-1} \quad (7.35) \quad \text{or ...} \quad T \cdot p^{\frac{\gamma}{1-\gamma}} = T \cdot p^{-\frac{\gamma}{\gamma-1}} = \text{constant} \quad [W 2.47]$$

$$T \cdot v^{\gamma-1} = \text{constant} \quad [W 2.48]$$

to explore the effect of temperature on the coefficients of specific heat the following is provided

to calculate enthalpies at non-standard conditions one approach is to use constant-pressure specific heats from Table A.9 of Van Wylen and Sonntag ... The applicable temperature range for these materials is 300 - 3500 deg K with less than approximately 0.5 % maximum error to experimental values. see also figure 5.10 on page 103.

$$\theta = \frac{T}{100} \quad \begin{matrix} T \text{ in deg} \\ K \end{matrix}$$

O2 $C_{po_O2}(\theta) := 37.432 + 0.020102 \cdot \theta^{1.5} - 178.57 \cdot \theta^{-1.5} + 236.88 \cdot \theta^{-2} \quad \frac{\text{kJ}}{\text{kmol} \cdot \text{K}}$

C_O2 $C_{po_C_O2}(\theta) := -3.7357 + 30.529 \cdot \theta^{0.5} - 4.1034 \cdot \theta + 0.024198 \cdot \theta^2 \quad \frac{\text{kJ}}{\text{kmol} \cdot \text{K}}$

N2 $C_{po_N2}(\theta) := 39.060 - 512.79 \cdot \theta^{-1.5} + 1072.7 \cdot \theta^{-2} - 820.40 \cdot \theta^{-3} \quad \frac{\text{kJ}}{\text{kmol} \cdot \text{K}}$

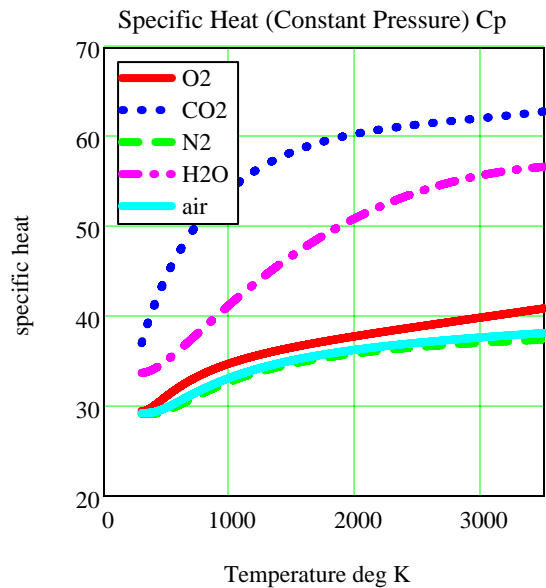
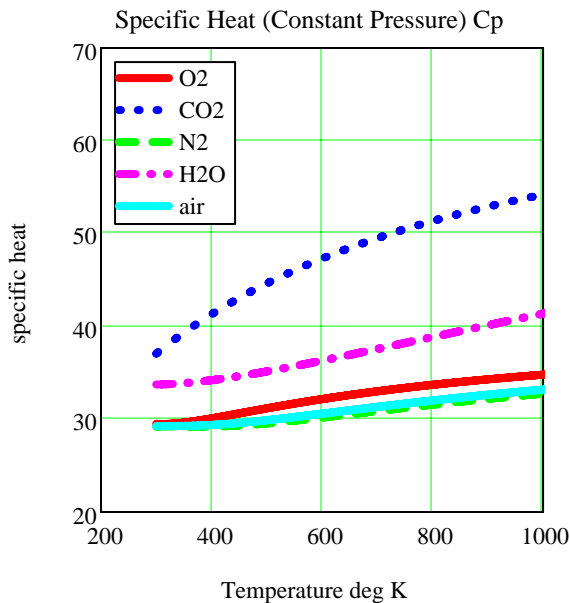
H2_O $C_{po_H2_O}(\theta) := 143.05 - 183.54 \cdot \theta^{0.25} + 82.751 \cdot \theta^{0.5} - 3.6989 \cdot \theta \quad \frac{\text{kJ}}{\text{kmol} \cdot \text{K}}$

given in kJ/kmole*K so divide by molecular weight to get kJ/kg*K

air based on volumetric average as these are on mole basis ...

air $C_{po_air}(\theta) := 0.21 \cdot C_{po_O2}(\theta) + 0.79 \cdot C_{po_N2}(\theta)$

$\bar{M}_w := 300 \dots 3500$



relatively constant at reasonably low temperatures

the next section was added Nov 2005 to organize plots for Brayton and dual (Seiliger) cycles

applications of above relationships to processes

$$R := 0.287 \quad \gamma := 1.4 \quad c_{po} := 1.0035 \quad \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \quad c_{vo} := \frac{c_{po}}{\gamma} \quad c_{vo} = 0.717$$

units assumed are p = bar, v = m³/kg, T = K, s = kJ/kg*K
 100 necessary for consistency in numerical calculations without units.

isentropic adiabatic compression (expansion)
pressure ratio known

$$P_{\text{initial}} := 1 \quad T_{\text{initial}} := 400 \quad s_{\text{initial}} := 1 \quad v_{\text{initial}} := \frac{R \cdot T_{\text{initial}}}{P_{\text{initial}} \cdot 100} \quad v_{\text{initial}} = 1.148$$

$$P_{\text{final}} := 10 \quad T_{\text{final}} := T_{\text{initial}} \left(\frac{P_{\text{final}}}{P_{\text{initial}}} \right)^{\frac{\gamma-1}{\gamma}} \quad s_{\text{final}} := s_{\text{initial}} \quad v_{\text{final}} := v_{\text{initial}} \left(\frac{P_{\text{initial}}}{P_{\text{final}}} \right)^{\frac{1}{\gamma}}$$

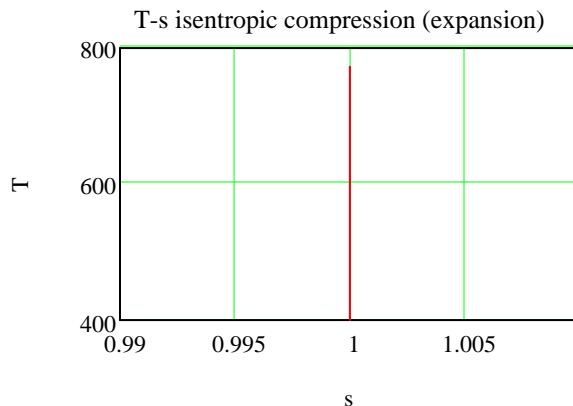
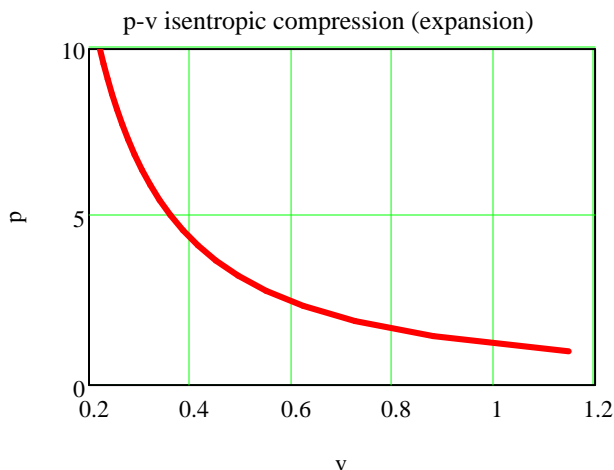
$$T_{\text{final}} = 772.279 \quad s_{\text{final}} = 1 \quad v_{\text{final}} = 0.222$$

p - v plot parameterized on either p or v say p

$$\delta p := \frac{P_{\text{final}} - P_{\text{initial}}}{20} \quad \text{to plot 20 points and accomodate increases and decreases}$$

$$PP := P_{\text{initial}} + \delta p \cdot i \quad T - s \text{ is straight line, need 2 points}$$

$$v_{\text{plot}}(PP) := v_{\text{initial}} \left(\frac{P_{\text{initial}}}{PP} \right)^{\frac{1}{\gamma}} \quad Ts_{\text{plot}} := \begin{pmatrix} T_{\text{initial}} & s_{\text{initial}} \\ T_{\text{final}} & s_{\text{final}} \end{pmatrix} \quad Ts_{\text{plot}} = \begin{pmatrix} 400 & 1 \\ 772.279 & 1 \end{pmatrix}$$



isentropic adiabatic compression (expansion)
volume ratio known

$$v_{\text{initial}} := 1 \quad T_{\text{initial}} := 400 \quad s_{\text{initial}} := 1 \quad P_{\text{initial}} := \frac{R \cdot T_{\text{initial}}}{v_{\text{initial}} \cdot 100} \quad P_{\text{initial}} = 1.148$$

$$v_{\text{final}} := \frac{1}{10} \quad T_{\text{final}} := T_{\text{initial}} \cdot \left(\frac{v_{\text{initial}}}{v_{\text{final}}} \right)^{\gamma-1} \quad s_{\text{final}} := s_{\text{initial}} \quad P_{\text{final}} := P_{\text{initial}} \cdot \left(\frac{v_{\text{initial}}}{v_{\text{final}}} \right)^{\gamma}$$

$$T_{\text{final}} = 1.005 \times 10^3 \quad s_{\text{final}} = 1 \quad P_{\text{final}} = 28.836$$

p - v plot parameterized on either p or v say p

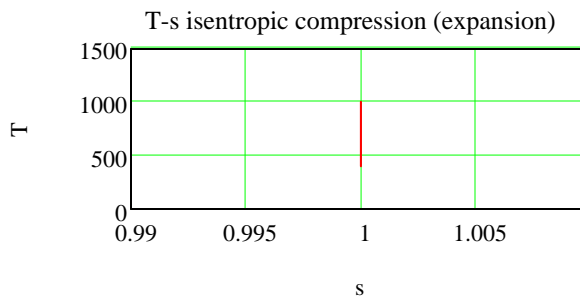
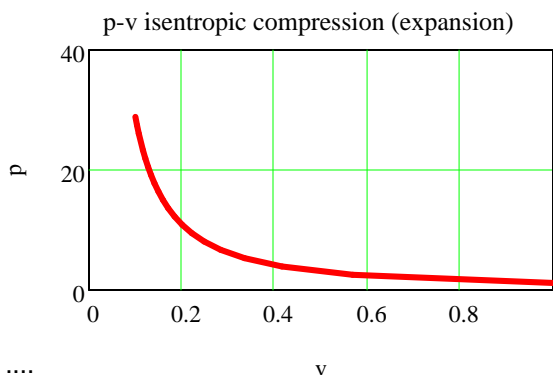
$$\delta p := \frac{P_{\text{final}} - P_{\text{initial}}}{20} \quad \text{to plot 20 points and accomodate increases and decreases}$$

$$pp := P_{\text{initial}} + \delta p \cdot n$$

T - s is straight line, need 2 points

$$pv_plot(pp) := v_{\text{initial}} \cdot \left(\frac{P_{\text{initial}}}{pp} \right)^{\frac{1}{\gamma}}$$

$$Ts_plot := \begin{pmatrix} T_{\text{initial}} & s_{\text{initial}} \\ T_{\text{final}} & s_{\text{final}} \end{pmatrix} \quad Ts_plot = \begin{pmatrix} 400 & 1 \\ 1.005 \times 10^3 & 1 \end{pmatrix}$$

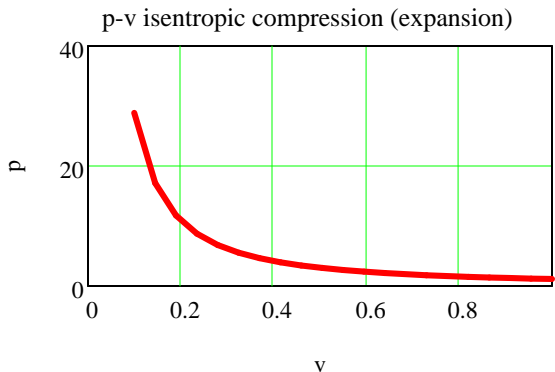


or

$$\delta v := \frac{v_{\text{final}} - v_{\text{initial}}}{20} \quad \text{to plot 20 points and accomodate increases and decreases}$$

$$vv := v_{\text{initial}} + \delta v \cdot n$$

$$pv_plot(vv) := P_{\text{initial}} \cdot \left(\frac{v_{\text{initial}}}{vv} \right)^{\gamma}$$



same plot as above

heat transfer at constant pressure

set up to go from T_{initial} to T_{final} at $p = \text{constant}$, s_{initial} assumed = 1

$$T_{\text{initial}} := 298 \quad s_{\text{initial}} := 1 \quad p_{\text{constant}} := 3 \text{ bar} \quad v_{\text{initial}} = 1$$

$$T_{\text{final}} := 500 \quad \text{final end state calculation}$$

$$s_{\text{final}} := s_{\text{initial}} + c_{\text{po}} \cdot \ln\left(\frac{T_{\text{final}}}{T_{\text{initial}}}\right) \quad s_{\text{final}} = 1.519 \quad v_{\text{final}} = 0.1$$

inbetween states for plotting

p - v is a straight line
needing only end
points to plot

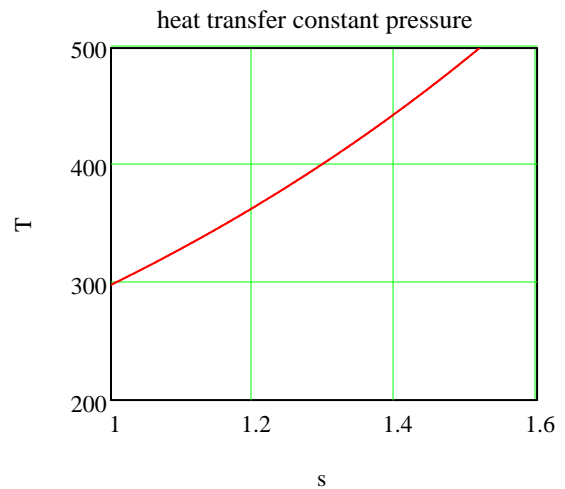
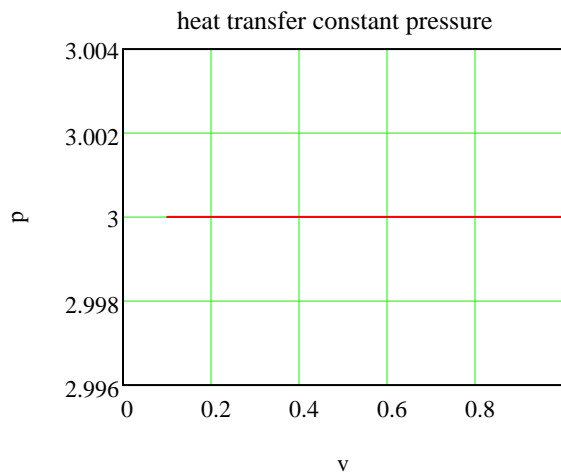
$$pv_plot := \begin{pmatrix} p_{\text{constant}} & v_{\text{initial}} \\ p_{\text{constant}} & v_{\text{final}} \end{pmatrix}$$

$$pv_plot = \begin{pmatrix} 3 & 1 \\ 3 & 0.1 \end{pmatrix}$$

if desired for a simulation where interim p v points are required, choose one parameter, e.g. T or v and calculate v or T using $pv/T = R$ for the other

$$TT := T_{\text{initial}} \cdot T_{\text{final}}$$

$$s_{\text{plot}}(TT) := \left(s_{\text{initial}} + c_{\text{po}} \cdot \ln\left(\frac{TT}{T_{\text{initial}}}\right) \right)$$



heat transfer at constant volume ...

set up to go from T_{initial} to T_{final} at $v = \text{constant}$, s_{initial} assumed = 1

$$T_{\text{initial}} := 450 \quad s_{\text{initial}} := 1 \quad v_{\text{constant}} := 0.3 \quad P_{\text{initial}} := \frac{R \cdot T_{\text{initial}}}{v_{\text{constant}} \cdot 100} \quad P_{\text{initial}} = 4.305$$

$$T_{\text{final}} := 298 \quad \text{final end state calculation}$$

$$s_{\text{final}} := s_{\text{initial}} + c_{v0} \cdot \ln\left(\frac{T_{\text{final}}}{T_{\text{initial}}}\right) \quad s_{\text{final}} = 0.705 \quad P_{\text{final}} := \frac{R \cdot T_{\text{final}}}{v_{\text{constant}} \cdot 100} \quad P_{\text{final}} = 2.851$$

inbetween states for plotting

p - v is a straight line
needing only end
points to plot

$$pv_plot := \begin{pmatrix} P_{\text{initial}} & v_{\text{constant}} \\ P_{\text{final}} & v_{\text{constant}} \end{pmatrix}$$

$$pv_plot = \begin{pmatrix} 4.305 & 0.3 \\ 2.851 & 0.3 \end{pmatrix}$$

if desired for a simulation where interim p v points are required, choose one parameter, e.g. T or v and calculate v or T using $pv/T = R$ for the other

$$TT := T_{\text{initial}} \cdot T_{\text{final}}$$

$$s_{\text{plot}}(TT) := \left(s_{\text{initial}} + c_{v0} \cdot \ln\left(\frac{TT}{T_{\text{initial}}}\right) \right)$$

